

**VISVESVARAYA TECHNOLOGICAL UNIVERSITY,
BELGAUM**

B.L.D.E. Association's

**VACHANA PITAMAHA Dr. P. G. HALAKATTI COLLEGE
OF ENGINEERING & TECHNOLOGY,**



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**DEPARTMENT OF
MECHANICAL ENGINEERING**

A PROJECT REPORT ON

**STUDY OF HEAT TRANSFER THROUGH CIRCULAR DUCT
WITH INSERTIONS (SPIRAL RIB INSERTIONS) AND
DETERMINING THE LOCAL HEAT TRANSFER COEFFICIENT
(SPONSORED BY KSCST AND I.I.Sc., BANGALORE)**

**UNDER THE GUIDANCE OF
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INTRODUCTION

Heat exchangers have several industrial and engineering applications. The design procedure of heat exchangers is quite complicated, as it needs exact analysis of heat transfer rate and pressure drop estimations apart from issues such as long-term performance and the economic aspect of the equipment. The major challenge in designing a heat exchanger is to make the equipment compact and achieve a high heat transfer rate using minimum pumping power. Techniques for heat transfer augmentation are relevant to several engineering applications. In recent years, the high cost of energy and material has resulted in an increased effort aimed at producing more efficient heat exchange equipment. Furthermore, sometimes there is a need for miniaturization of a heat exchanger in specific applications, such as space application, through an augmentation of heat transfer. For example, a heat exchanger for an ocean thermal energy conversion (OTEC) plant requires a heat transfer surface area of the order of 10000 m²/MW. Therefore, an increase in the efficiency of the heat exchanger through an augmentation technique may result in a considerable saving in the material cost. Furthermore, as a heat exchanger becomes older, the resistance to heat transfer increases owing to fouling or scaling. These problems are more common for heat exchangers used in marine applications and in chemical industries. In some specific applications, such as heat exchangers dealing with fluids of low thermal conductivity (gases and oils) and desalination plants, there is a need to increase the heat transfer rate. The heat transfer rate can be improved by introducing a disturbance in the fluid flow (breaking the viscous and thermal boundary layers), but in the process pumping power may increase significantly and ultimately the pumping cost becomes high.